### Research Needs for Carbon Capture and Mitigation

University of Kentucky Center for Applied Energy Research

> Rodney Andrews Director Email: andrews@caer.uky.edu Tel: 859/ 257-0200

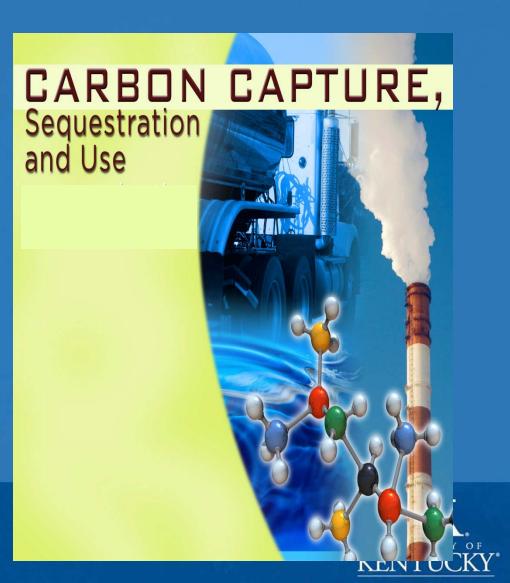
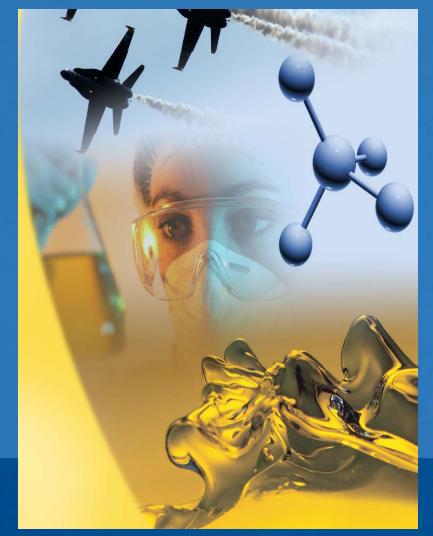


Photo art: A. Benlow

see blue.

# Agenda



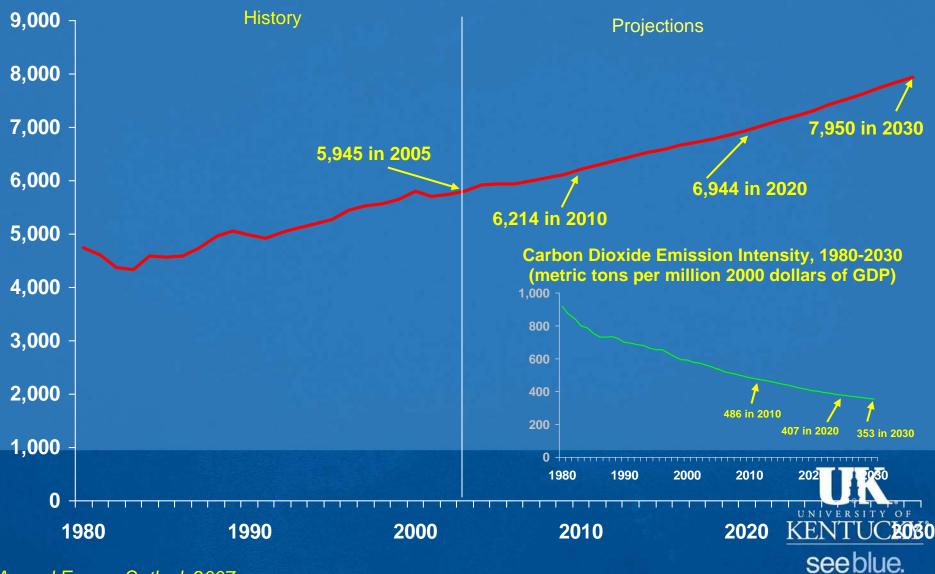
 Extent and Sources of CO<sub>2</sub> Emissions
 Management & Capture

• Research Needs

Photo art: A. Benlow

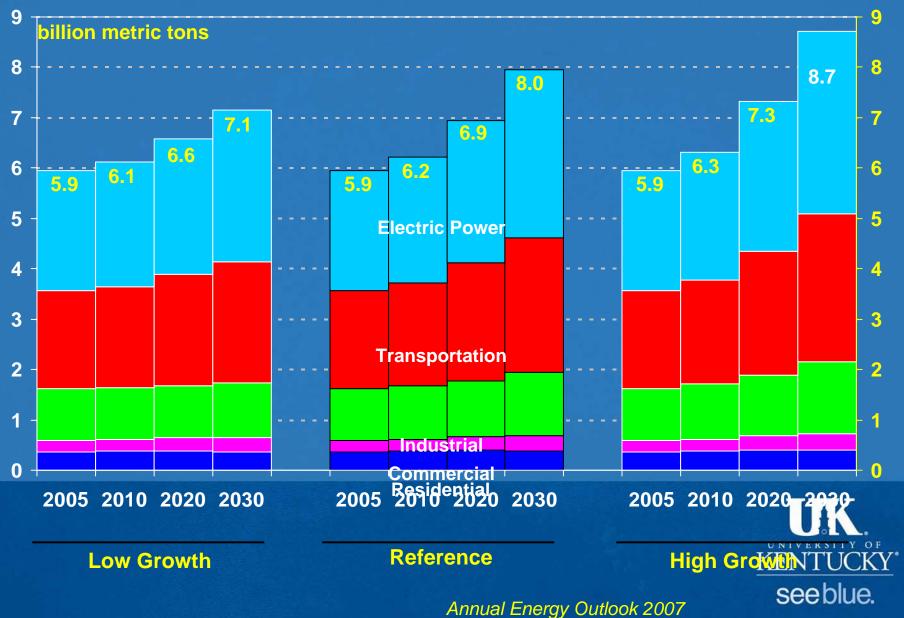


### U.S. Energy-Related Carbon Dioxide Emissions, 1980-2030 (million metric tons)

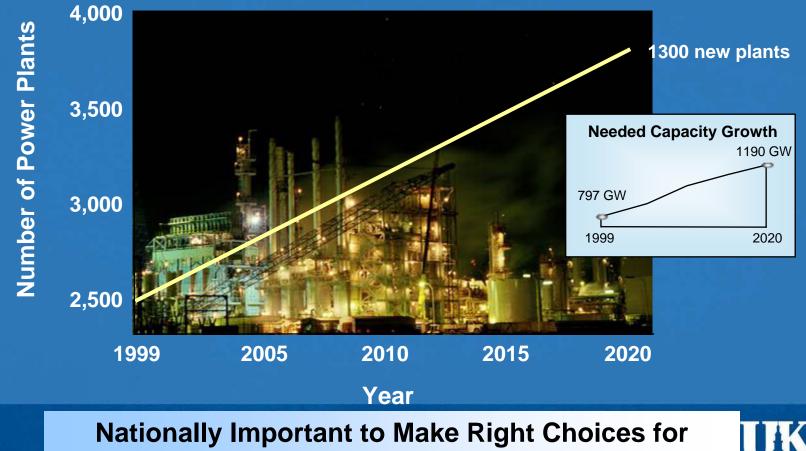


Annual Energy Outlook 2007

# **Carbon Dioxide Emissions**



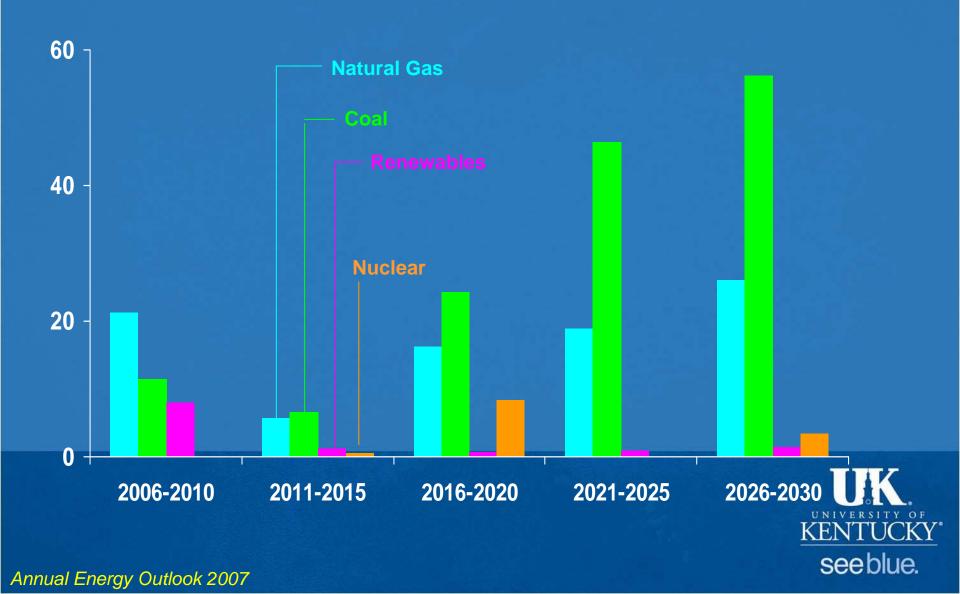
### Needed: 1,300 New Power Plants A Conservative Estimate

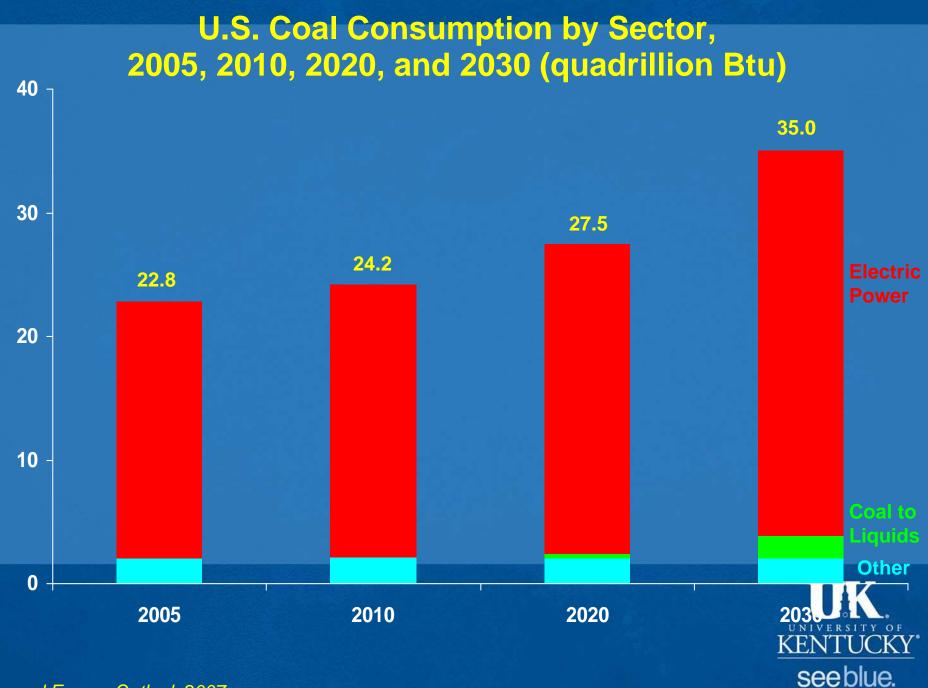


Infrastructure Investments With 50+ Year Lifetime

Source: EIA/D&Eeeblue.

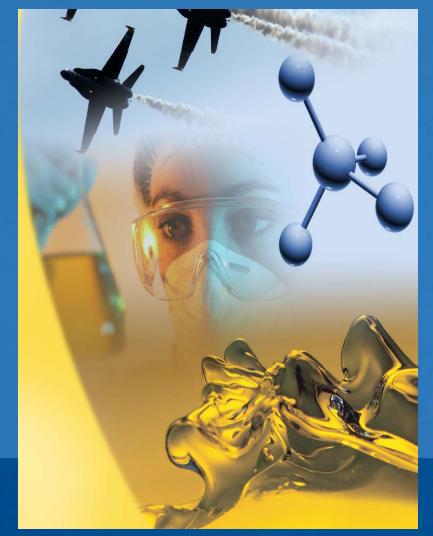
### U.S. Electricity Generation Capacity Additions by Fuel, 2006-2030 (gigawatts)





#### Annual Energy Outlook 2007

# Agenda

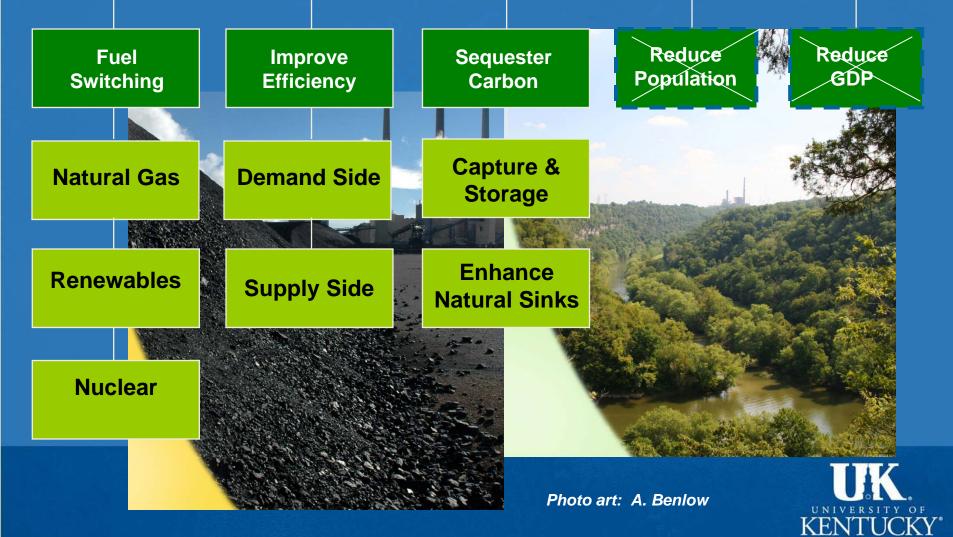


Extent and Sources of CO<sub>2</sub> Emissions
 Management & Capture
 Research Needs

Photo art: A. Benlow

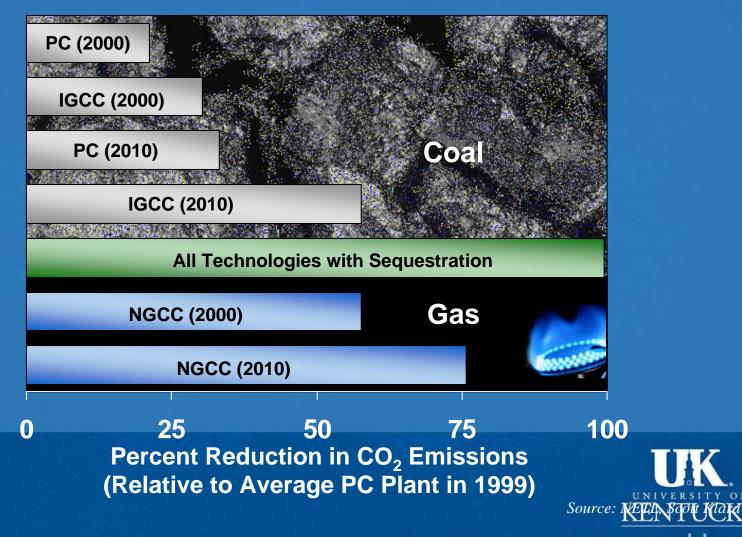


### **Technology and Innovation** Can Lead to Reductions in Carbon Emissions



see blue.

### Reductions in Carbon Emissions By Adoption of New Power Generation Technologies



see blue.

### Reductions in Carbon Emissions By Switching to Natural Gas

#### Era of "Cheap" Gas May Be Over

#### • Supply cushion since mid-1980's eroded

- US supply flat past 5 years
- Rapid decline curves for new wells
- Canadian gas/LNG imports up from 4% in mid-1980s to 15%
- Spot Market Prices up 4-fold
- Projected 2-3% annual growth – up 60% thru 2020
- T&D infrastructure stressed
  - Need \$120-150B investment to expand system





Source: USDOE

Reductions in Carbon Emissions By Switching to Renewables

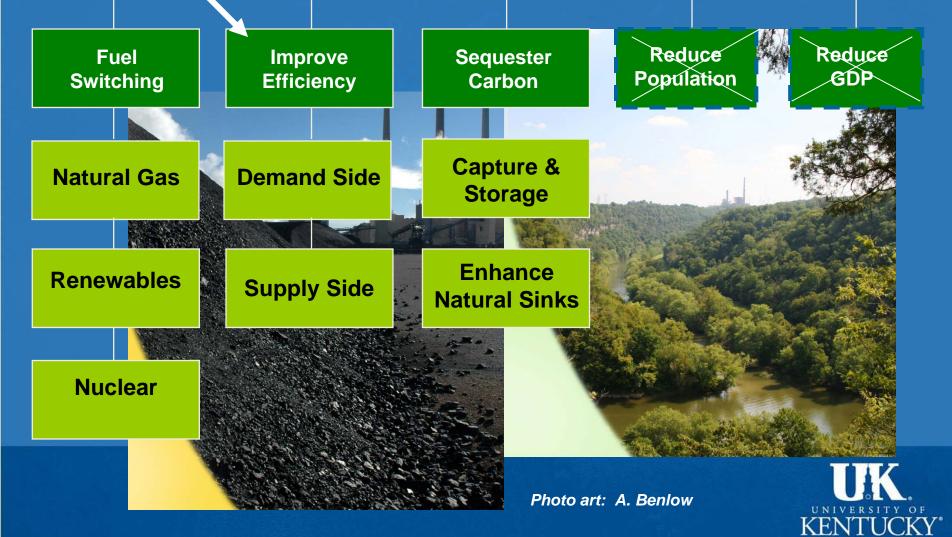
Wind, hydro, and geothermal - Not enough Biomass -Transportation, land use, expense Solar - Land use, capital cost, storage



Needed: An Affordable, Clean, and Abundant Energy Source No Known Source Meets These Criteria

Source: USDOE SEE blue.

### **Technology and Innovation** Can Lead to Reductions in Carbon Emissions



see blue.

### Reductions in Carbon Emissions By Demand-side Efficiency



Insulate your house
Thermal windows
High efficiency appliances
Water-saving devices
Natural lighting/solar mass

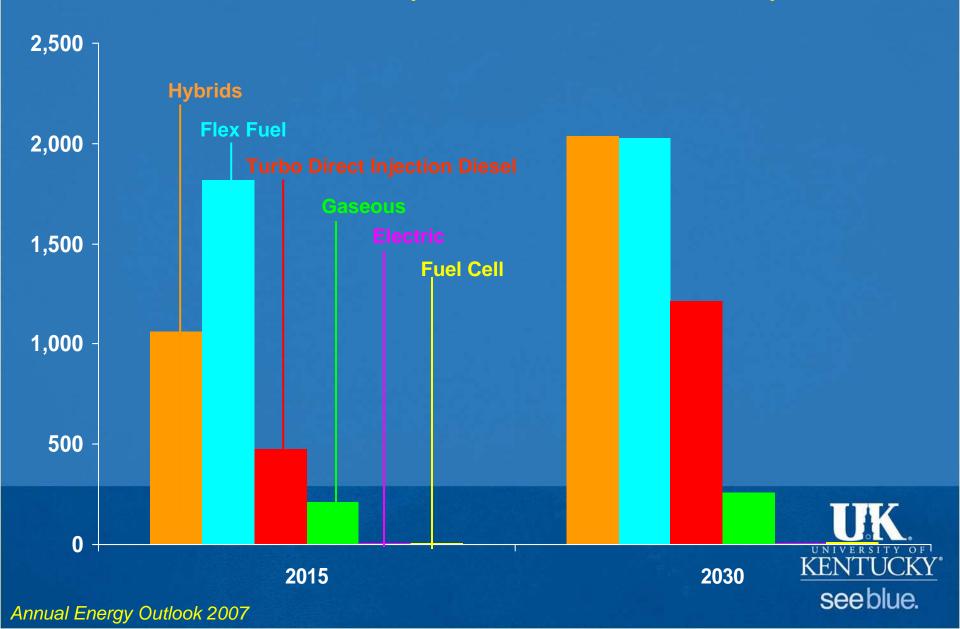




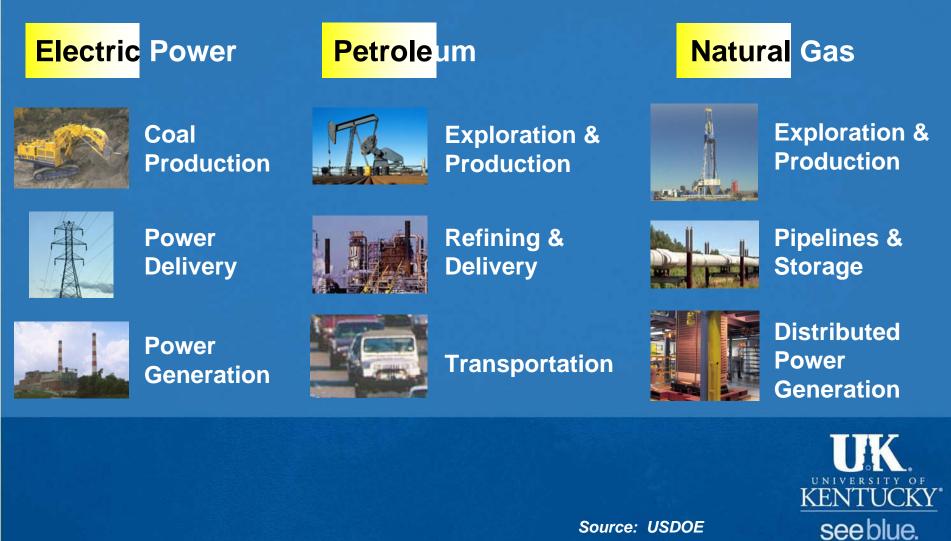
Eat lower on the food chain
Get close to your food

Encourage industrial efficiency
"Green" chemistry
Recycle your waste Park your SUV
Take the Bus
Higher Price at the Pump
Demand CAFÉ
Buy the "Hybrid" KENTUCKY see blue.

#### U.S. Sales of Unconventional Light-Duty Vehicles, 2015 and 2030 (thousand vehicles sold)



**Reductions in Carbon Emissions** By Greater Supply-side Efficiency

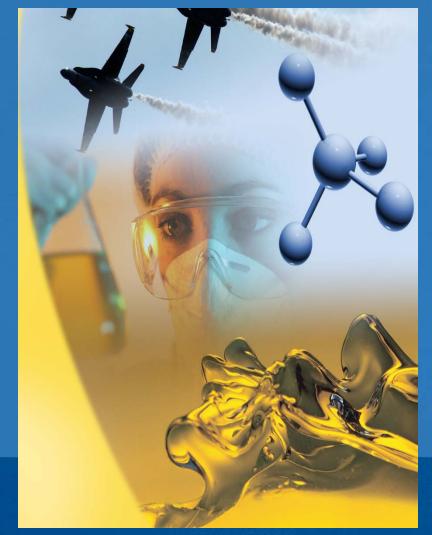


### **Technology and Innovation** *Can Lead to Reductions in Carbon Emissions*



Photo art: A. Benlow

# Agenda



Extent and Sources of CO<sub>2</sub> Emissions
 Management & Capture
 Research Needs

Photo art: A. Benlow



### **Technology and Innovation** *Can Lead to Reductions in Carbon Emissions*

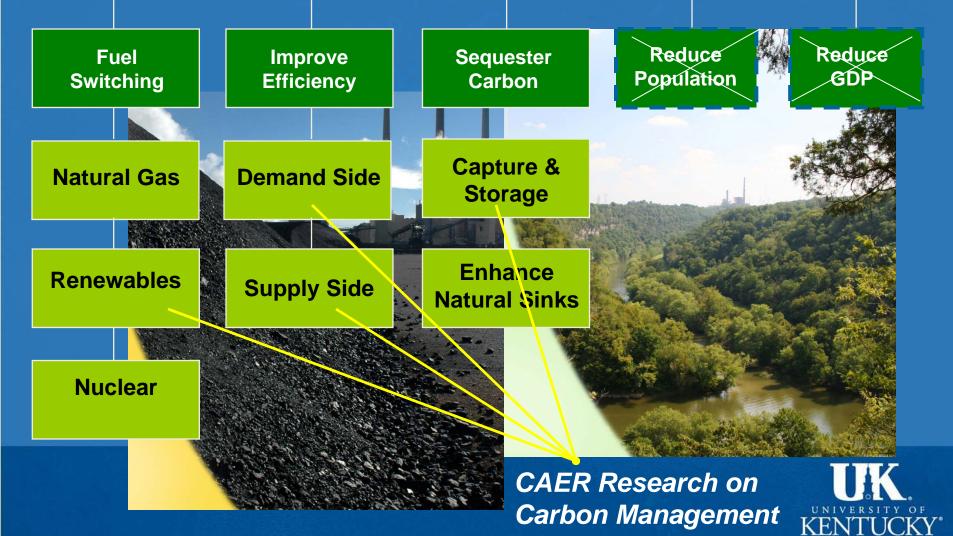
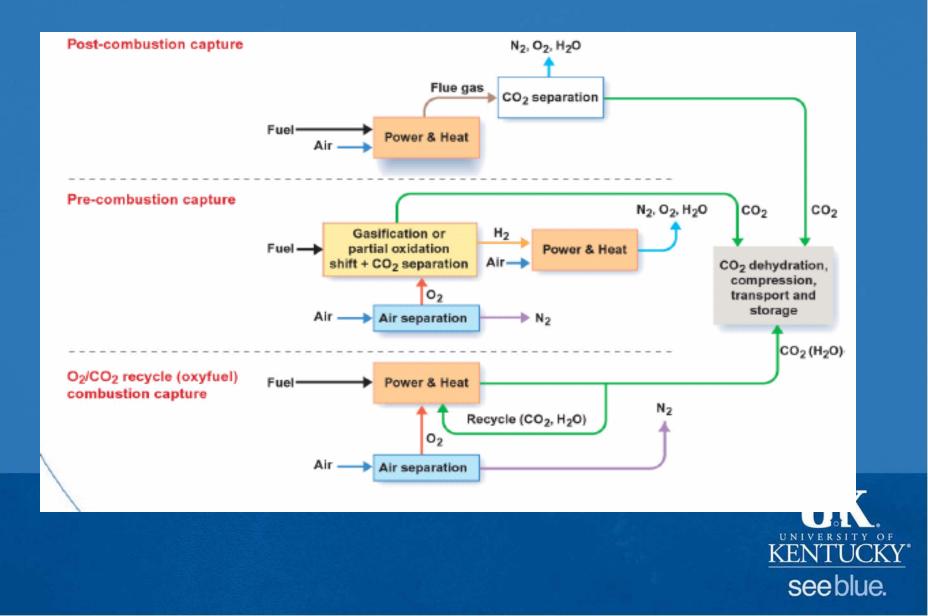


Photo art: A. Benlow

see blue.

### **CO<sub>2</sub> Capture from Electricity Generation**

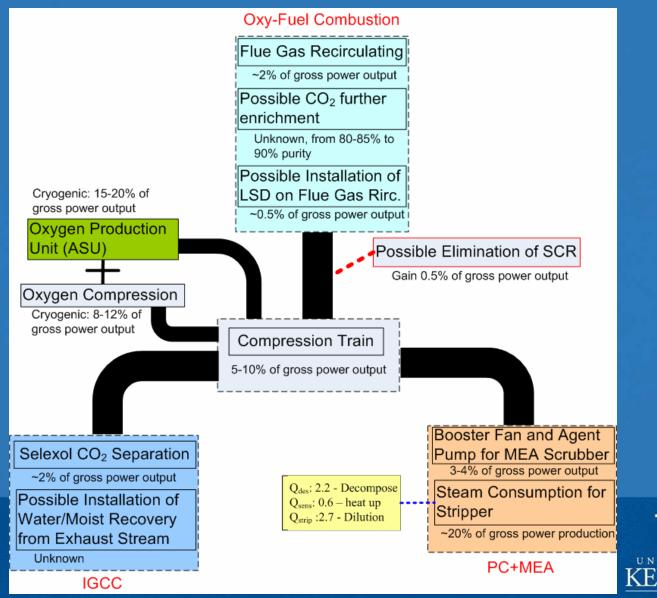


### Research directed to Lowering Energy Penalty of CO<sub>2</sub> Capture Options

- Post-Combustion Capture: PC + MEA (28-34%)
  - Steam consumption for stripper: 20% of gross power output
  - Booster fan and agent pump for MEA scrubber: 3-4% of gross power output
- Pre-combustion Capture: IGCC (total 15-24%)
  - ASU + oxygen compression: 8-12% of gross power output
  - Selexol CO<sub>2</sub> separation: 2% of gross power output
- In-situ Capture: Oxy-Fuel Combustion (total 22-32%)
  - ASU: 15-20% of gross power output
  - Flue gas recirculation: 2% of gross power output
  - Possible CO2 further enrichment (unknown)
- \*\* Compression Train: 5-10% of gross power output



### **Possible Choices for CO2 Management**



KENTUCKY seeblue.

# Current Status of IGCC

- Mature technology for gasifier
- New wave pushed by GE, Shell and ConocoPhillips
- OEMs teamed with engineering companies to wrap
- RD&D
  - New catalyst/shift-reactor process to reduce H<sub>2</sub>O/CO ratio
  - Membrane separation
  - Sorbent development
  - Process integration
  - Oxygen production



# **Current Status of Oxy-Fuel**

- Oxyfuel -- Commercial available for glass, steel and other sectors
  - Demo
    - Praxair & Foster Wheeler
      - Bahamas project
      - Fundación Ciudad de la Energía (CIUDEN)
    - B&W and Air Liquide
      - SaskPower (terminated?)
      - AEP
    - Alstom
      - Vattenfall
  - Ongoing RD&D for Utility
    - Vattenfall 30MWe plant
    - Air Liquide/B&W 4MMBtu and 40MMBtu plant
    - Alstom (3MWth FBC)
    - Universität Stuttgart (0.5MWth PC)
    - CANMET (0.3MWth PC and 1.0MWth FBC)
  - Air Separation Unit
    - Ion transport membrane (ITM) (Air Products, Praxair)
    - Ceramic autothermal recovery (CAR) (BOC Gases)



# Post CO<sub>2</sub> Capture Process

- Absorption Processes (Liquid & Solid)
- Adsorption Process (Solid Surface, Ionic Liquid)
- Physical Separation (Membrane, Cryogenic Separation)
- Hybrid Solution (Mixed Physical Chemical Solvent)



# Post Combustion Scrubbing in Fossil Power Plants

### •Challenges:

- Low CO<sub>2</sub> partial pressure
  - 5-15 vol%
- Low System Pressure
- 25-35% of plant output for auxiliary power.

### •Capital Costs \$500/kW

- Three absorbers with same diameter as FGD, 50 ft packing.
- Strippers somewhat smaller.



# **Physical Absorption**

•Physical solvent processes use organic or inorganic solvents to physically absorb acid gas components rather than react chemically.

•Removal of CO<sub>2</sub> by physical absorption processes based on the solubility of CO<sub>2</sub> within the solvents.

•The solubility of CO<sub>2</sub> depends on the partial pressure and on the temperature of the feed gas.

•Regeneration of the spent solvent can be achieved by flashing to lower pressure or by stripping with vapor or inert gas.



# **Chemical Absorption**

• Chemical absorption processes are based on exothermic reaction of the solvent with the  $CO_2$  in the feed gas stream.

• Chemical reaction must be reversible. The reactive solvent removes  $CO_2$  in the absorber at low temperature. The reaction is then reversed by endothermic stripping process at high temperature and low pressure.

 Majority of chemical solvent processes use either an amine or carbonate solution.

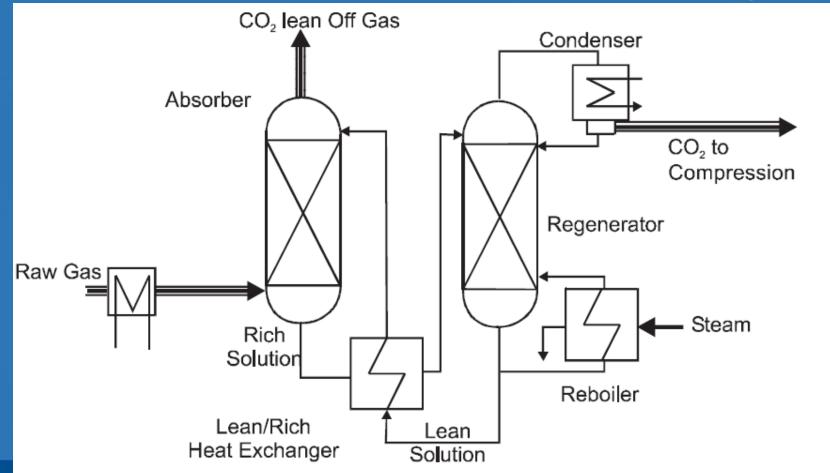


# **Chemical Absorption Processes**

- Potassium Carbonate.  $K_2CO_3 + CO_2 + H_2O \leftrightarrow 2KHCO_3$
- Monoethanolamine (MEA) 2 HO-CH<sub>2</sub>-CH<sub>2</sub>-NH<sub>2</sub> + CO<sub>2</sub>  $\leftrightarrow$ HO-CH<sub>2</sub>-CH<sub>2</sub>-NH-COO<sup>-</sup> + MEAH<sup>+</sup>
- Ammonia  $2NH_3 + CO_2 \leftrightarrow NH_2COO^- + NH_4^+$



## **Chemical Absorption Scrubbing**





# **Reagent Properties Affecting Makeup**

	Cost \$/lbmol	P <sub>amine, 40C</sub> atm x 10 <sup>3</sup>	Degradation	Corrosion
MEA	40	0.1	High	High
NH <sub>3</sub>	5	200	None	High
PZ	300	0.1	Moderate	High
MDEA	300	0.003	Moderate	Moderate
K <sub>2</sub> CO <sub>3</sub>	40	0	None	High

Source: Rochelle, 2007



### **Current Status of Aqueous Scrubbing**

• Amine: commercial-implementation on NG, food and chemical production

- Kerr-McGee/ABB Lummus Crest Process
- Fluor Daniel ECONAMINE FG Process
- MHI's KM-CDR process with KS solvent
- Ongoing RD&D for utility flue gas
  - University of Texas at Austin
  - European Union integrated project "CO<sub>2</sub> from Capture to Storage" (CASTOR)
  - International Test Center (ITC) at University of Regina, Canada
  - MHI
  - UK CAER
- Ammonia: Commercial for fertilizer production
  - Ongoing RD&D for Utility's flue gas
    - Alstom/EPRI 5MWth pilot plant at WE Energy Pleasant Prairie Plant
    - Powerspan/NETL 1MWth slipstream at FirstEnergy's Burger station
    - UK CAER/E-ON US 0.1MWth pilot plant



# **CAER CO<sub>2</sub> Capture Research**

- •Two Supported by E-ON US:
- \*Post-Combustion Process
  - Solvent-based CO<sub>2</sub> capture technologies
  - New concept development
    - Solid additives
    - Membrane for solution separation
- \*In-situ process (No external ASU)
  - Pressurized Chemical Looping Combustion Combined Cycle (PCLC-CC)
- •Two for existing PC supported by GOEP
  - Feasibility Study on Using Algal Capture and Utilize CO<sub>2</sub> Source from Kentucky Power Plants
  - Development of Liquid Membrane for Solvent-Based Post-Combustion CO<sub>2</sub> Scrubber
- •One for IGCC supported by CAER
  - Activated Carbons for CO<sub>2</sub> Capture from Coal-derived Pitch/Polymer Blends



### Solvent-based CO<sub>2</sub> Capture Pilot-plant Objectives

- Provide a flexible pilot-scale platform to study a variety of CO<sub>2</sub> scrubbing processes for existing power stations.
- Study and optimize the power requirements for CO<sub>2</sub> scrubbing technologies.
- Solvent development and solvent management protocol (impact from coal impurities).
- Material Corrosion



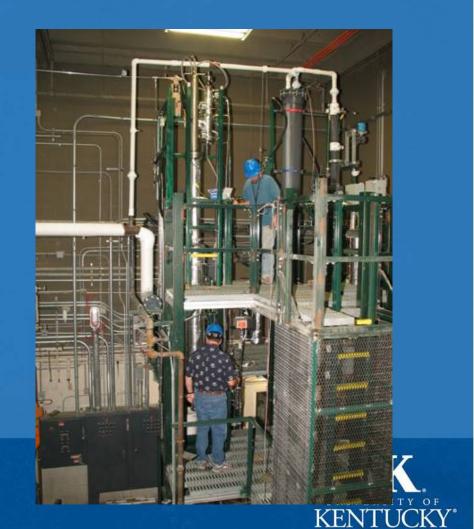
# 0.1MWth Post-combustion CO<sub>2</sub> Capture Pilot Plant

#### • Scrubber with height of 22-25 ft:

- 10" bottom tank, a 4" reaction zone, and a 8" reaction zone
- Flexible configuration (open, tray-type or packed column)

#### • Stripper with height of 15ft

- 8" for reboiler section, 4" tower
- 400°F and 450 psia (max)
- Range of gas flows: 10-50 scfm
- L/G range: 50 to 200
- Simulated flue gas
  - mixed from N<sub>2</sub>, air, CO<sub>2</sub>, HCl and SOx tanks.
- Will work on coal-derived flue gas
- generator



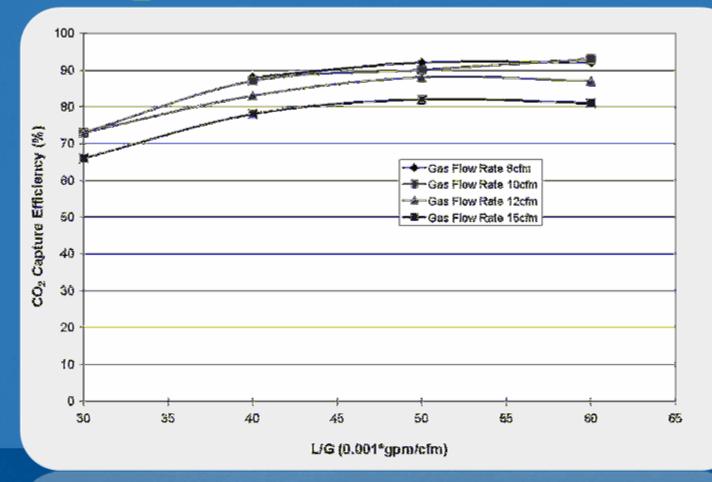
see blue.

### **Research Progress**

- •Completed commissioning using K2CO3 Solvent -Easy solvent
- -Under utility flue gas cond., the CO2 removal efficiency at 3%-10%
- Pre-trail Study using K<sub>2</sub>CO<sub>3</sub>/Piperizane (PZ)
  - solution preparation difficult (solved)
- low PZ solubility in lean solution (Precipitation of PZ at low Temp)
- 100 hrs run using 1.5m K<sub>2</sub>CO<sub>3</sub>/PZ
  •Baseline Testing using 30% MEA
  •Over two-month with 32 runs using ceramic packing
  -foaming in stripper
  -MEA degradation vs. stripping temperature
  -Metal concentration profile



# CO<sub>2</sub> capture vs. L/G Ratio

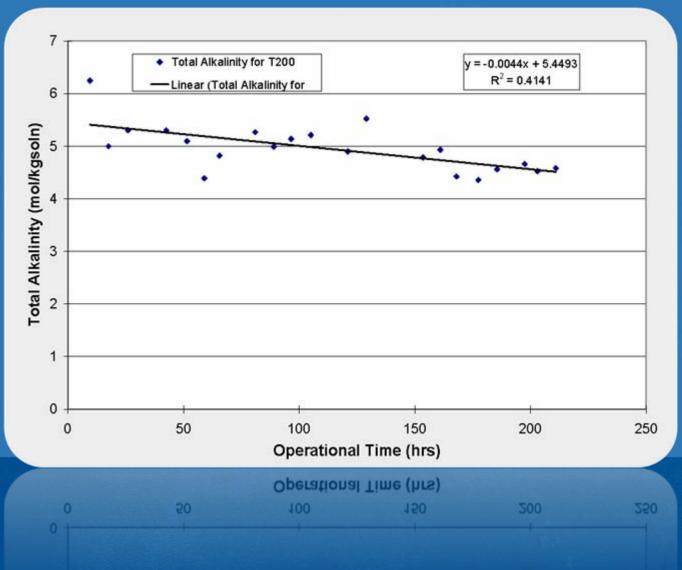


L/G (0.901\*gpm/chn)

20



# **MEA Degradation vs. Time**



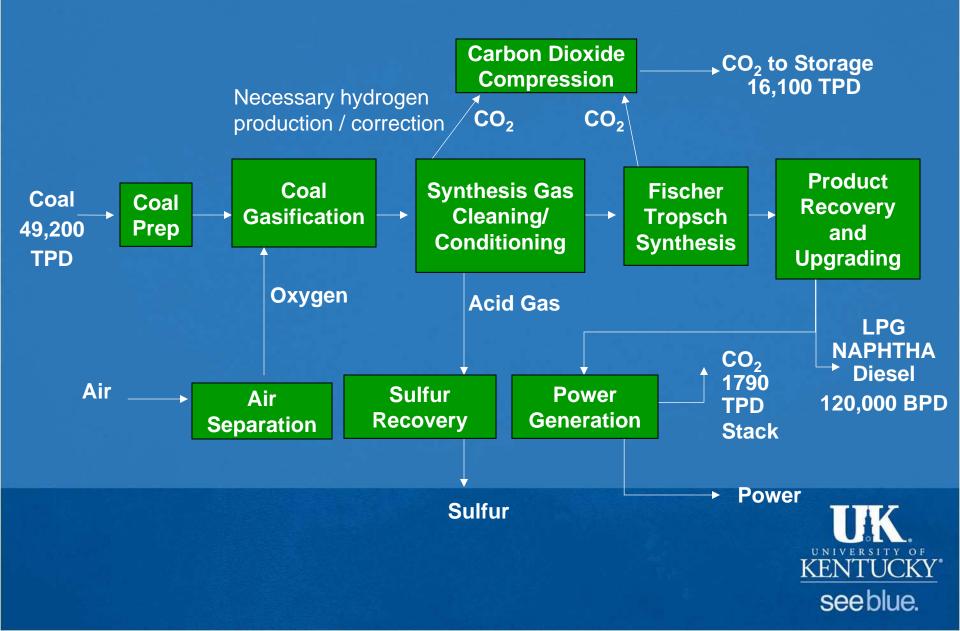


### Carbon Management Research Group

- State-UK-Industry consortium
- Build on E-ON US investment in carbon management and emissions control
- Develop more energy and cost effective carbon management technologies
- Address specific materials, controls and waste management solutions
- Allow early adoption of technologies by Kentucky's electric utilities
- \$1 Million/yr match provided by State.



### CO<sub>2</sub> Capture from Coal-to-Liquids



## Mitigating Carbon Impact from the Production of FT Fuels

- Enhanced modular reactor systems
- Improved catalysts for water-gas-shift
   <u>– Reduce unwanted CO2</u> formation
- Use of biomass in FT processes
  - Biomass gasification
  - Gas cleaning
  - Utilization of biomass as hydrogen source
- Co-feed of Coal and Biomass for CTL







Graphic: Future Gen, US DoE



Photo art: A. Benlow

KENTUCKY see blue.